Copyright is owned by the Author of the thesis. Permission is given for a copy to be downloaded by an individual for the purpose of research and private study only. The thesis may not be reproduced elsewhere without the permission of the Author.

THE PREDICTION OF DRYING TIME OF EXPANDED POLYSTYRENE BLOCKS

A thesis presented in partial fulfilment of the requirements for the degree of

Master of Technology in Production Technology at

Massey University

Yan Li

1998



Abstract

A study of methods to predict the drying time of expanded polystyrene was made with the aim of optimizing the drying conditions of the drying kiln at Lanwood Industries.

Experiments were carried out in both a laboratory and Lanwood Industries factory. The drying rate was found to decrease with increasing product thickness and to increase with increasing drying temperature. Drying temperature between 50 and 60 °C has a stronger influence on the EPS drying process than between 40 and 50 °C.

A simplified theoretical method can be used to predict the drying time in the industrial environment when quick computation is needed. Newton's model can fit the full-scale drying process, but it did not fit the laboratory drying processes well. Page's model has an excellent fit to the three dimensional EPS drying process and it is also able to scale up the laboratory drying results. It supplies a powerful tool to describe the drying process and predict the drying time of the EPS product.

Acknowledgements

I would like to express my sincere thanks to my supervisor, Mr P Collins for his guidance, encouragement and friendship throughout this study and also for his constructive criticism and correction of my English during all the discussions.

I would like to thank Mr D Houston and Mr J Dawber for their help, kindness and suggestions on my written English during the writing of this thesis.

I also would like to thank Dr W Page, Dr C Marsh and Mr H Barraclough for their valuable suggestions on the data analysis of this study.

I am particularly grateful to Mr J Lockwood and Mr S Thompson of Lanwood Industries for their support of the providing drying samples and facilities.

I wish to thank all staff and postgraduate students of Production Technology

Department and the staff of Lanwood Industries for their friendship and help offered.

Finally, I wish to express my deep gratitude to my parents and my sister for their love and encouragement. Also, I thank all my friends for their continual support and helpfulness.

Table of Contents

Title	i
Abstract	ü
Acknowledgements	
Table of Contents	iv
List of Figures	
List of Tables	ix
Chapter 1 Introduction	1
Chapter 2 Review of Existing Knowledge and Background Theory	3
2.1 Basic theory	4
2.1.1 General principles	
2.1.2 Drying rates and drying curves	4
2.1.3 Critical moisture content	7
2.1.4 Equilibrium moisture content	8
2.2 Factors affecting the air drying	10
2.2.1 External conditions	10
2.2.1.1 Temperature	10
2.2.1.2 Relative humidity	
2.2.1.3 Air velocity	11
2.2.2 Internal conditions	
2.2.2.1 Physical properties of solids	12
2.2.2.2 Temperature	17
2.2.2.3 Moisture content	17
2.3 Drying models and calculations	18
2.3.1 Pure diffusion model	18
2.3.2 Semitheoretical drying equations	24
2.3.3 Empirical drying equations	26

Chapter 3 Materials and Experimental Work	30
3.1 EPS products	
3.1.1 Materials	31
3.1.2 EPS production processes	
3.1.2.1 Expansion	31
3.1.2.2 Drying	33
3.1.2.3 Cutting expanded polystyrene	34
3.2 Drying experiments	35
3.2.1 Drying samples	35
3.2.2 Equipment	36
3.2.2.1 Drying cabinet	
3.2.2.2 Drying kiln	38
3.2.3 Measurements	
3.2.3.1 Laboratory drying measurements	43
3.2.3.2 Full-scale drying measurements	.53
3.2.4 Discussion of experimental results	57
Chapter 4 Analysis and Modelling of the Drying process	60
4.1 Drying process analysis	61
4.1.1 Drying time in the constant-rate period	61
4.1.2 Falling-rate period	63
4.1.3 Final moisture content in industrial operation	.64
4.1.4 The results and discussion	66
4.2 Drying time prediction	68
4.2.1 Theoretical drying methods	69
4.2.1.1 The simplified method	69
4.2.1.2 Numerical method	73
4.2.2 Semitheoretical drying equation	
4.2.3 Empirical drying equation	.77
4.2.4 The results and discussion	80
4.3 Evaluation of the drying models	82
4.3.1 Limitations in accuracy and validity	82
4.3.2 The results and discussion	85

Chapter 5 Cor	nclusions and Recommendations86
5.1 Conclusion	s
5.2 Recommen	dations 88
Nomenclature .	90
References	92
Appendices	
Appendix A	Variation of the density distribution
Appendix B	Variation of the moisture content
Appendix C	Buoyancy effects on the EPS block weight during drying 105
Appendix D	Comparison of experimental data and Newton's equation
Appendix E	Comparison of experimental data and Page's equation

List of Figures

Figure	2.1	Drying curves	5
Figure	2.2	The pre-expanded beads and final moulded polystyrene beads	14
Figure	2.3	Four stages of moisture migration in the drying of a porous material	. 15
		The drying cabinet	
Figure	3.2	The Lanwood kiln ductwork	. 39
Figure	3.3	Diagram of the air flow in Lanwood drying kiln	. 40
Figure	3.4	Air flow in a drying chamber	41
		A schematic diagram of the full-scale experimental apparatus	
Figure	3.6	Mean moisture content of thirty, 50 mm cubic EPS samples	
		versus time	45
Figure	3.7	Mean drying rate of thirty, 50 mm cubic EPS samples	
		versus moisture content	45
Figure	3.8	Moisture contents of different cubic sized samples versus time	
		at 50 °C	. 47
Figure	3.9	Moisture contents of three cubic sized samples versus time	
		at 40 °C	49
Figure	3.10	Moisture contents of three cubic sized samples versus time	
		at 50 °C	49
Figure	3.11	Moisture contents of three cubic sized samples versus time	
		at 60 °C	50
Figure	3.12	Drying rate of three cubic sized samples versus moisture content	
		at 40 °C	. 50
Figure	3.13	Drying rate of three cubic sized samples versus moisture content	
		at 50 °C	.51
Figure	3.14	Drying rate of three cubic sized samples versus moisture content	
		at 60 °C	.51
Figure	3.15	Moisture contents of 100 mm cube samples versus time	
		at 40, 50 and 60 °C	52

Figure	3.16Moisture contents of 200 mm cube samples versus time	
	at 40, 50 and 60 °C	52
Figure	3.17Moisture contents of 250 mm cube samples versus time	
	at 40, 50 and 60 °C	53
Figure	3.18The weight of an EPS block versus time in the full-scale test	55
Figure	3.19Moisture content of an EPS block versus time in the full-scale test 5	55
Figure	3.20The drying rate of an EPS block versus moisture content	
	in the full-scale test5	56
Figure	4.1 The drying parameter k of Newton's equation versus Area/Volume 7	16
Figure	4.2 The drying parameter k of Page's equation versus Area/Volume	18
Figure	4.3 The drying parameter N of Page's equation versus Area/Volume	19
Figure	A The sample position in an EPS block	2
Figures	s D.1 to D.10 Comparison of experimental data and Newton's equation10)6
Figures	s E.1 to E.10 Comparison of experimental data and Page's equation 11	1

List of Tables

Table 3.1 The shrinkage of an EPS block after drying	56
Table 4.1 Values of the drying curves in the laboratory tests	67
Table 4.2 The slopes of drying-rate curves in the first falling-rate period	72
Table 4.3 The drying parameter k of Newton's equation in each test run	74
Table 4.4 The drying parameter k and N of Page's equation in each test run	77

Chapter 1 Introduction

This project, which has been done in conjunction with Lanwood Industries of Palmerston North, was supervised by Mr. Phil Collins from the Production Technology Department at Massey University. The research intends to improve the drying quality of expanded polystyrene (EPS) blocks used as insulation by the construction industry.

The processing of the EPS product employs a pre-expansion stage where steam is blown through raw polystyrene beads which contain a small amount of pentane. The partly expanded beads from this stage are called "prefoam". Before moulding the prefoamed beads are put into large hoppers to dry. After drying, the material is then blown into a mould and treated again with steam to soften the prefoamed bead for final fusing. Blocks of EPS leaving the moulder contain both pentane (the expanding agent) and up to 10 % moisture from the steam injected during moulding. Before hot wires cut the blocks into slabs, the blocks are dried in warm air chambers to allow the pentane and moisture to disperse. Residual pentane can cause a fire hazard during cutting. If too much moisture remains in the block, the cutting wires cool down which causes an uneven cut surface, drag marks or "picture framing". Moisture also has other adverse effects, such as detaching the outer layer of composite panels and reducing the insulation efficiency.

The purpose of this project is to determine the optimum conditions for drying moisture from moulded EPS, in order to minimise the drying time while also maintaining acceptable product surface quality during the hot-wire cutting. Both laboratory drying tests and full-scale drying tests were carried out to study the drying process of the EPS product.

In EPS block (3.6m×1.2m×0.65m) drying, moisture movement occurs along the length, width and height of the block which involves three dimensional drying. In order to simulate the full-scale drying process, drying samples were cut into a cubic shape

from fresh moulded EPS blocks and dried in a laboratory drying cabinet. These results together with drying theory were used to scale up the laboratory experimental data to the full-scale drying operation. The capillary theoretical method, Newton's model and Page's model were used for the drying time calculation.

Some limitations encountered during the data collection and analysis were: the varying drying conditions during the full-scale tests, the limited experimental data, and the large gap in dimensions of drying materials between the laboratory tests and the full-scale tests. The scale-up procedures are by no means straight forward. However, Page's equation was found to give a better fit for the experimental data of both the laboratory and the full-scale tests. Page's model is able to describe the three dimensional drying process of the EPS product. It also provides a method to scale up the laboratory results for the optimization of the drying conditions.